



Boundaries_LL_NRTL

Graphical User Interface (GUI) for the Characterization of the NRTL Model: Binary Spinodal Surfaces (in the $\tau_{i,j}-\tau_{j,i}-x_i$ space), LLE Maps, and Miscibility Boundaries

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Juan A. Labarta*, M. Mar Olaya and Antonio Marcilla

Department of Chemical Engineering & Institute of Chemical Process Engineering. University of Alicante, Apdo. Correos 99, 03080 Alicante, Spain.

* Contact details for more information and/or comments.

Corresponding author: ja.labarta@ua.es

ORCID : <http://orcid.org/0000-0002-4870-2031>

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1. INTRODUCTION

In a similar way to the previous MatLab Graphical User Interfaces (GUI's) developed to systematically check the consistency of LLE or VLE data correlation results, [GMcal_TieLinesLL](#) [1,2] [GMcal_TieLinesVL](#) [3] respectively, this Graphical User Interface (**Boundaries_LL_NRTL**) has been developed as a friendly tool for the analysis of the NRTL model, and it is directly related with the *AICHE Journal* research paper: ***“What does the NRTL model look like? Determination of boundaries for different fluid phase equilibrium regions”*** [4]. This GUI allows the direct visualization and calculation of 3D representations (in the $\tau_{i,j}-\tau_{j,i}-x_i$ space) and 2D projections (in the $\tau_{i,j}-\tau_{j,i}$ plane) of binary spinodal surfaces, LLE maps, and miscibility boundaries of the NRTL model for different values of the non-randomness parameter ($\alpha_{i,j}$) between 0 and 0.95.

The analysis of all these figures allows researchers involved in the correlation of experimental liquid-liquid equilibrium data, to establish relations between the typology of the system under study (regarding the behavior of all the binary subsystems) and the values of the NRTL binary interaction parameters $\tau_{i,j}-\tau_{j,i}$ consistent with that typology.

NRTL model for non-ideal liquid mixtures

➤ **Gibbs energy of mixing**

$$g^{M(L)} = G^{Mixture,L}/RT = G^{Ideal}/RT + G^{Excess}/RT = x_i \cdot \ln(x_i) + G^E/RT$$

➤ **Excess Gibbs energy:**

$$\frac{G^E(NRTL)}{RT} = \sum_{i=1}^C x_i \cdot \frac{\sum_{j=1}^C \tau_{j,i} \cdot G_{j,i} \cdot x_j}{\sum_{k=1}^C G_{k,i} \cdot x_k}$$

➤ **Activity coefficient:**

$$\ln \gamma_i = \frac{G^E}{RT} + \sum_{j=1}^C x_j \cdot \left(\frac{\partial(G^E/RT)}{\partial x_i} - \frac{\partial(G^E/RT)}{\partial x_j} \right)$$

$$\ln \gamma_i^{NRTL} = \frac{\sum_{j=1}^C \tau_{j,i} \cdot G_{j,i} \cdot x_j}{\sum_{k=1}^C G_{k,i} \cdot x_k} + \sum_{j=1}^C \frac{G_{i,j} \cdot x_j}{\sum_{k=1}^C G_{k,j} \cdot x_k} \cdot \left(\tau_{i,j} - \frac{\sum_{m=1}^C \tau_{m,j} \cdot G_{m,j} \cdot x_m}{\sum_{k=1}^C G_{k,j} \cdot x_k} \right)$$

with $\tau_{j,i} = \frac{A_{j,i}}{RT}$; $G_{j,i} = \exp(-\alpha_{j,i} \cdot \tau_{j,i})$; $A_{i,i}=0$ and $\alpha_{i,j} = \alpha_{j,i}$

For a binary system ($C=2$):

$$\frac{G^E(NRTL)}{RT} = x_1 \cdot \frac{\tau_{21} \cdot G_{21} \cdot x_2}{x_1 + G_{21} \cdot x_2} + x_2 \cdot \frac{\tau_{12} \cdot G_{12} \cdot x_1}{G_{12} \cdot x_1 + x_2}$$

$$\frac{\partial(G^E(NRTL)/RT)}{\partial x_1} = \frac{\tau_{21} \cdot (G_{21} \cdot x_2)^2}{(x_1 + G_{21} \cdot x_2)^2} + \frac{\tau_{12} \cdot G_{12} \cdot x_2^2}{(G_{12} \cdot x_1 + x_2)^2}$$

$$\frac{\partial(G^E(NRTL)/RT)}{\partial x_2} = \frac{\tau_{21} \cdot G_{21} \cdot x_1^2}{(x_1 + G_{21} \cdot x_2)^2} + \frac{\tau_{12} \cdot (G_{12} \cdot x_1)^2}{(G_{12} \cdot x_1 + x_2)^2}$$

$$\ln \gamma_1^{NRTL} = x_2^2 \cdot \left[\frac{\tau_{21} \cdot G_{21}^2}{(x_1 + x_2 \cdot G_{21})^2} + \frac{\tau_{12} \cdot G_{12}}{(x_2 + x_1 \cdot G_{12})^2} \right]$$

$$\ln \gamma_2^{NRTL} = x_1^2 \cdot \left[\frac{\tau_{12} \cdot G_{12}^2}{(x_2 + x_1 \cdot G_{12})^2} + \frac{\tau_{21} \cdot G_{21}}{(x_1 + x_2 \cdot G_{21})^2} \right]$$

2. USER INSTRUCTIONS

1. Download instructions

1. Download the file to your computer in a known folder: [Boundaries_LL_NRTL.zip](#)
2. Unzip the file

2. Using the GUI Boundaries_LL_NRTL

1. Open Matlab software
2. Once in MatLab, select the folder where the file **Boundaries_LL_NRTL.zip** was unzipped as “current folder”.
3. Localize and execute the file **Boundaries_LL_NRTL.p** from the MatLab Command Window (i.e.: writing **Boundaries_LL_NRTL** in the Command Window, and pressing enter). The next windows will appear.

Boundaries_LL_NRTL: Graphical User Interface (GUI) for the Characterization of the NRTL Model:
Binary Spinodal Surfaces (in the $\tau_{ij}, \tau_{ji}, x_i$ space), LLE Maps and Miscibility Boundaries
 Chemical Engineering Department & Institute of Chemical Process Engineering, University of Alicante (Spain)**
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Visualization of pre-calculated binary spinodal surfaces, LLE maps and miscibility boundaries for the NRTL model (α_{ij} from 0 to 0.95):

$\alpha_{ij}=0$ $\alpha_{ij}=0.10$ $\alpha_{ij}=0.20$ $\alpha_{ij}=0.30$ $\alpha_{ij}=0.40$ $\alpha_{ij}=0.50$ $\alpha_{ij}=0.60$ $\alpha_{ij}=0.70$ $\alpha_{ij}=0.80$ $\alpha_{ij}=0.90$
 $\alpha_{ij}=0.05$ $\alpha_{ij}=0.15$ $\alpha_{ij}=0.25$ $\alpha_{ij}=0.35$ $\alpha_{ij}=0.45$ $\alpha_{ij}=0.55$ $\alpha_{ij}=0.65$ $\alpha_{ij}=0.75$ $\alpha_{ij}=0.85$ $\alpha_{ij}=0.95$
Summary 3DFig

Calculation of a specific NRTL binary spinodal surface and LLE maps (by discrete scanning):

τ_{ij} limits: +/-: Number of τ_{ij} points: Number of x_i points:
 α_{ij} value: Map Calculation Grid of individual gML curves

Representation of correlated miscibility boundaries for the NRTL model: (Ref.: [10] *AIChE Journal*, 2022, e17085)

k	t(1,k)	t(2,k)	t(3,k)	t(4,k)	$f(LLE)$	p(1)	p(2)	p(3)	p(4)	$f(mLLE)$	p(1)	p(2)	p(3)	p(4)	
LLE 0	-61.7182	144.834	-96.6099	9.89155	$(0.4 < \alpha_{ij} < 0.95)$	a(q)	0.17018	0.94122	-15.8026	7.41426	a(q)	0.17970	3.66704	-12.2321	-169.867
1	11.0599	-7.61356	2.78799	0.94847	$(0 < \alpha_{ij} < 0.4)$	b(q)	1.18745	0.38618	6.61230	8.99112	b(q)	0.04713	1.09335	-2.70716	-78.5291
2	-18.9354	46.0735	-37.9180	10.6231	$(0.4 < \alpha_{ij} < 0.95)$	c(q)	0.86617	0.08518	9.30456	0.54484	c(q)	0	0	0	0
mLLE 3	-712.144	769.320	-297.731	44.5980	$(0.15 < \alpha_{ij} < 0.43)$	d(q)	-1.29669	-2.15462	-2.06603	-11.2860	d(q)	-1.00726	-11.9808	66.6629	299.304
						e(q)	0.45992	1.95455	3.08991	3.68996	e(q)	2.93938	0.38653	-69.0533	-146.868

Correlated boundaries evolution: L-LLE Boundaries mLLE Boundaries

New single boundaries calculation: α_{ij} value: 0 < < 0.95 Boundaries calculation

Additional bibliography:

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 [11] GMcal_TieLinesVL: Graphical User Interface (GUI) for the Topological Analysis of Gibbs Energy Functions for Binary and Ternary (isobaric or isothermal) Vapor-Liquid Equilibrium (VLE) Data (including Tie-Lines, Derivatives, Distillation Boundaries, etc.) (RUA 2022): <http://hdl.handle.net/10045/122857>.

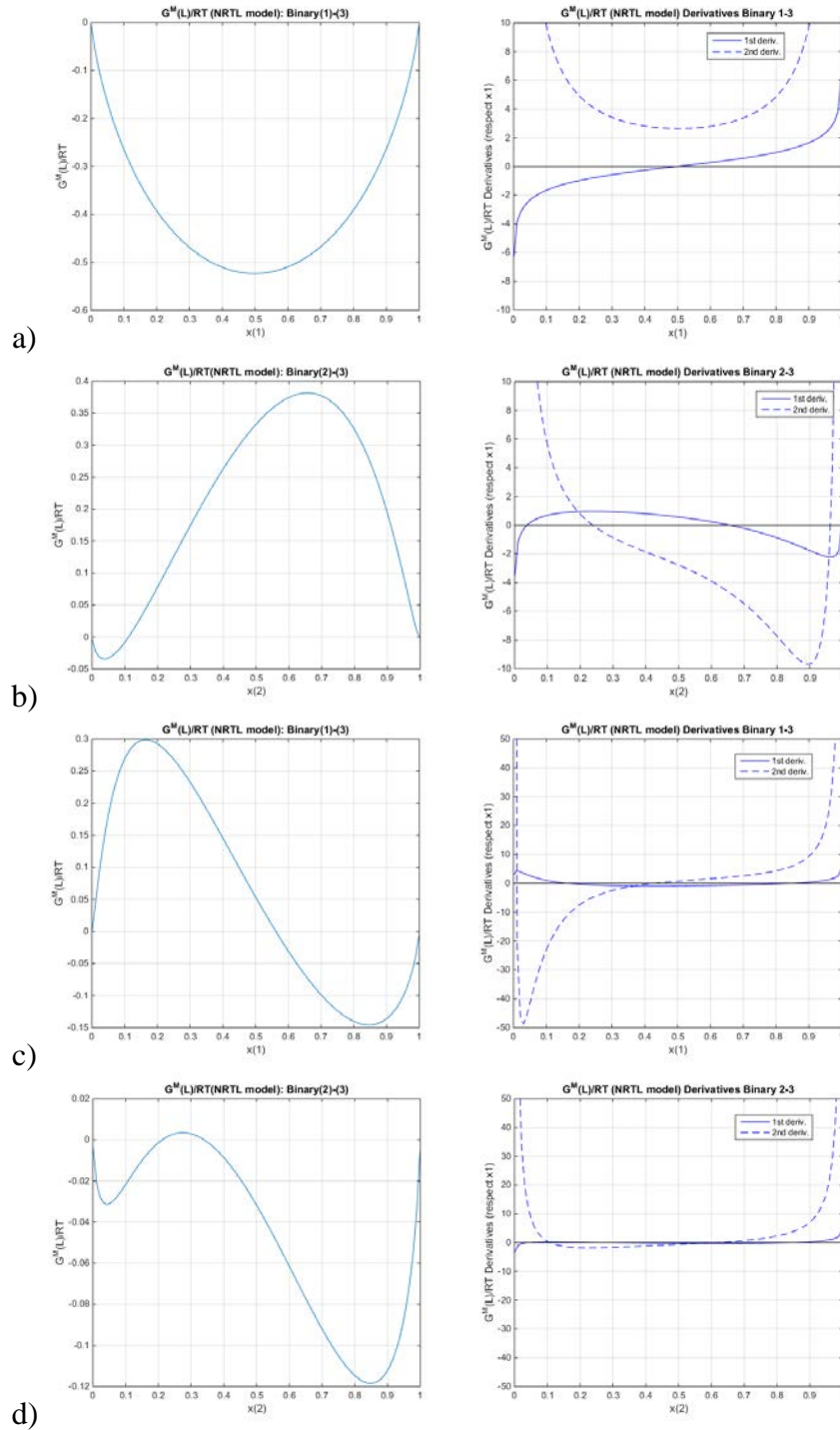
**Corresponding author (for more information or comments): ja.labarta@ua.es (ORCID: 0000-0002-4870-2031) Exit

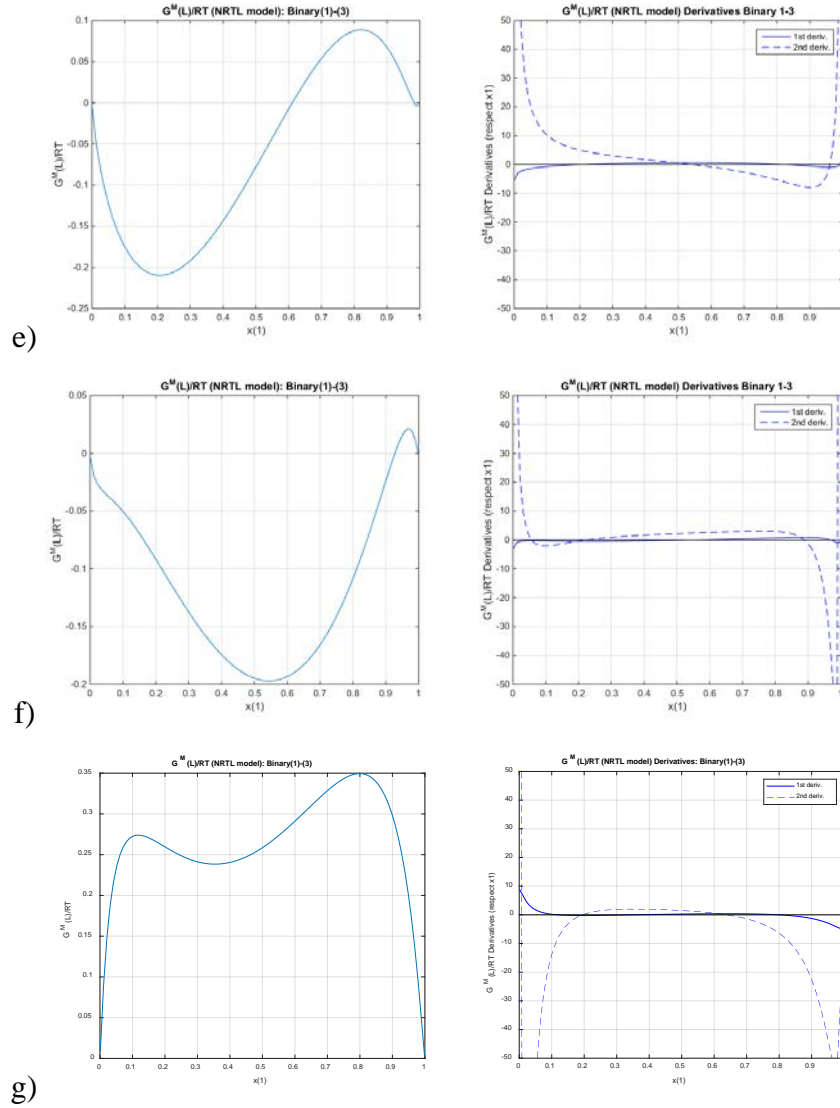
4. Once the main window of the GUI appears, it is possible to create different diagrams by using the corresponding push buttons:

- Pre-calculated 3D binary spinodal surfaces (in the $\tau_{i,j}-\tau_{j,i}-x_i$ space) and miscibility boundaries (2D projections in the $\tau_{i,j}-\tau_{j,i}$ plane) for the NRTL model for different $\alpha_{i,j}$ values (from 0 to 0.95). (e.g. Figures 1a).
- Figure 3D resume with all the 2D projections for different $\alpha_{i,j}$ values, from 0 to 0.95 (Figure 1b).
- Calculation and representation of a specific NRTL binary spinodal surface and its 2D projection for a concrete value of $\alpha_{i,j}$ (by discrete scanning of the binary parameters $\tau_{i,j}$ and $\tau_{j,i}$). It is possible to choose the $\alpha_{i,j}$ value, the upper/lower limits of the tau parameters, and the number of tau and x points used in the corresponding scanning. The default values are respectively: 0.2; +/- 10; 100 and 15000. (e.g. Figures 1c)

Remark: The possibility of the existence of LL phase splitting has been analyzed through zeros of the second derivative of the Gibbs energy of mixing (with respect to

the molar fraction), for each set of $\tau_{i,j}-\tau_{j,i}$ values, in the whole composition range ($x_i \in [0,1]$). That is due because the presence of a LL splitting requires the existence of two zeros in the second derivative of the Gibbs energy of mixing, as can be observed in the following figures: Case a represents a totally homogeneous binary mixture in the whole range of compositions, while cases b-e correspond to binary systems with two partially miscible components just one LLE. When there are more than two compositions with a value of zeros in the second derivative of the Gibbs energy of mixing, more than one LL splitting exists (case f or g):



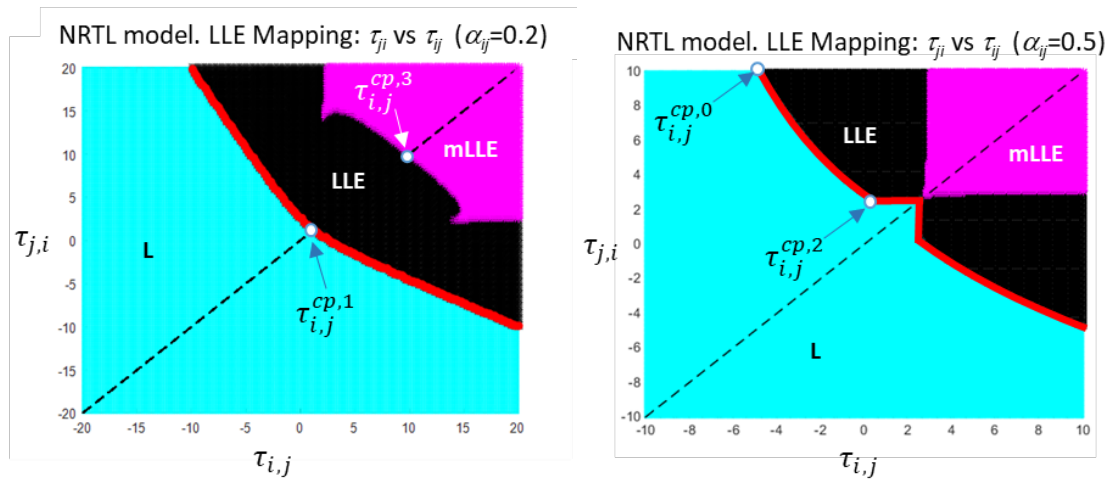


- Calculation and representation of a grid of individual Gibbs energy of mixing curves specific NRTL binary spinodal surface for a concrete value of $\alpha_{i,j}$ and different pairs of the binary parameters $\tau_{i,j}$ and $\tau_{j,i}$. (e.g. Figure 1d).
- Representation of the evolution of the correlated L-LLE and LLE-mLLE boundaries observed for the NRTL by using the set of parameters included as default corresponding with the following equations and definitions [3]) (Figures 1e).

$$f(\tau_{i,j}, \alpha_{i,j}) \equiv \tau_{j,i}^{cal} = p_1 \cdot \tau_{i,j}^3 + p_2 \cdot \tau_{i,j}^2 + p_3 \cdot \tau_{i,j} + p_4$$

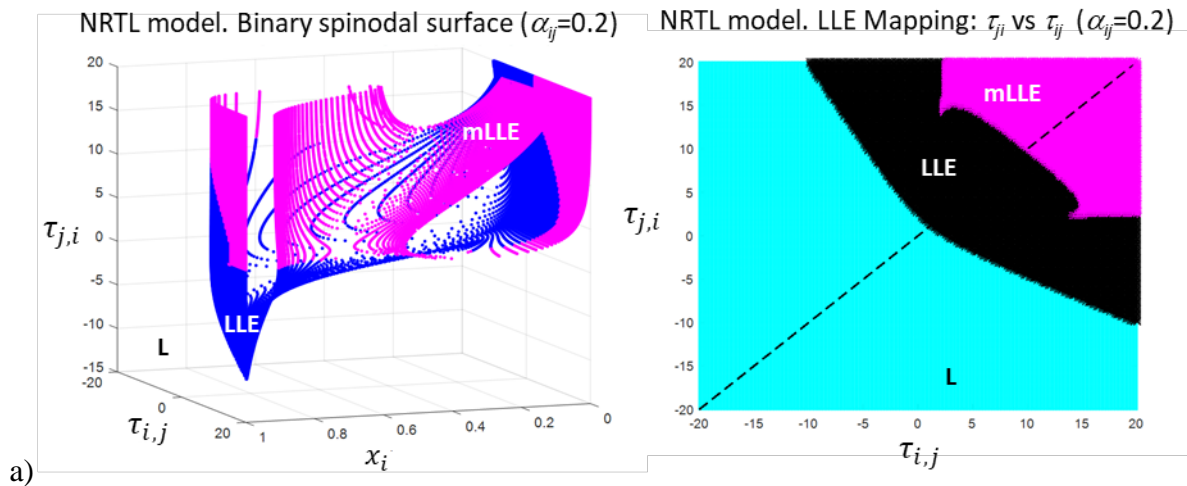
$$p_q = a_q + b_q \cdot \ln(\alpha_{i,j} + c_q) + d_q \cdot \alpha_{i,j} + e_q \cdot \alpha_{i,j}^2 \quad q = \{1,2,3,4\}$$

$$g_k(\alpha_{i,j}) \equiv \tau_{i,j}^{cp,k} = t_{1,k} \cdot \alpha_{i,j}^3 + t_{2,k} \cdot \alpha_{i,j}^2 + t_{3,k} \cdot \alpha_{i,j} + t_{4,k}$$

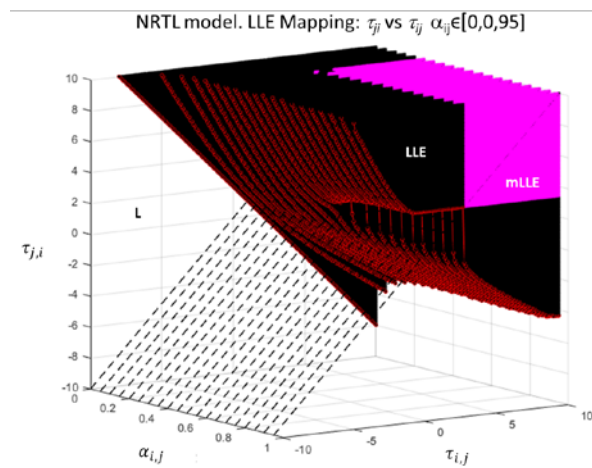


If we use the value of 10 as the upper bound for $\tau_{j,i}$, in both cases, the miscibility boundary (red line) exists in the range of values of $\tau_{i,j}$ from -5 to 10, i.e. $\tau_{i,j}^{cp,0} = -5$.

- Calculation and representation of the correlated NRTL miscibility boundaries for a specific value of $\alpha_{i,j}$ and different pairs of the binary parameters $\tau_{i,j}$ and $\tau_{j,i}$. (e.g. Figure 1f).

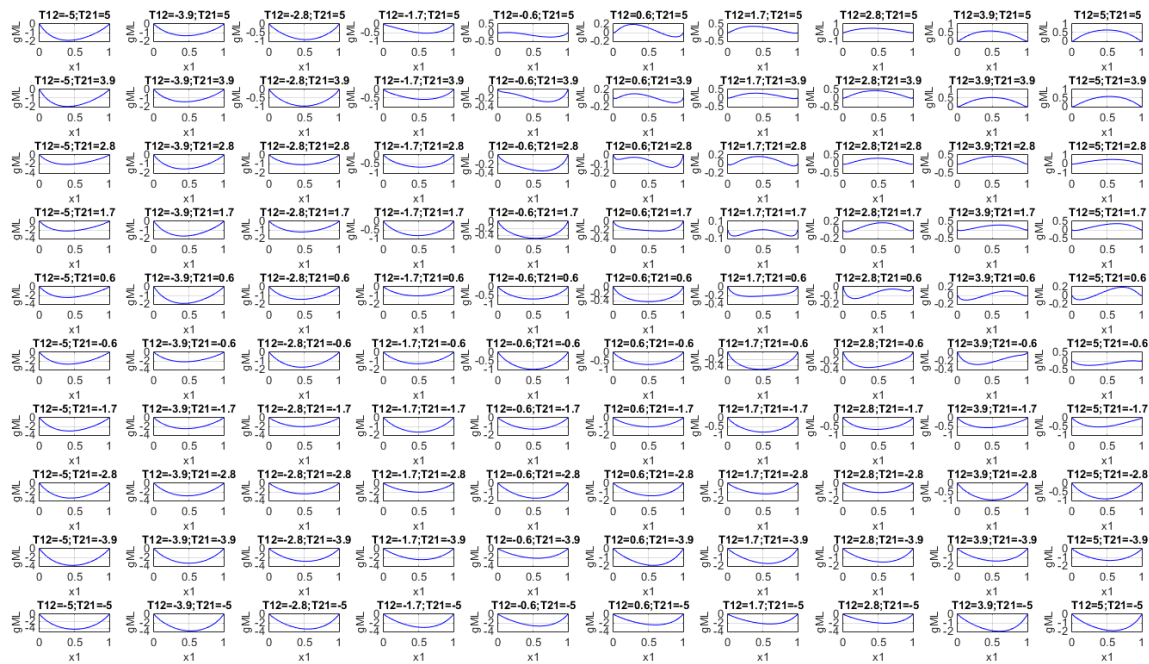


a)

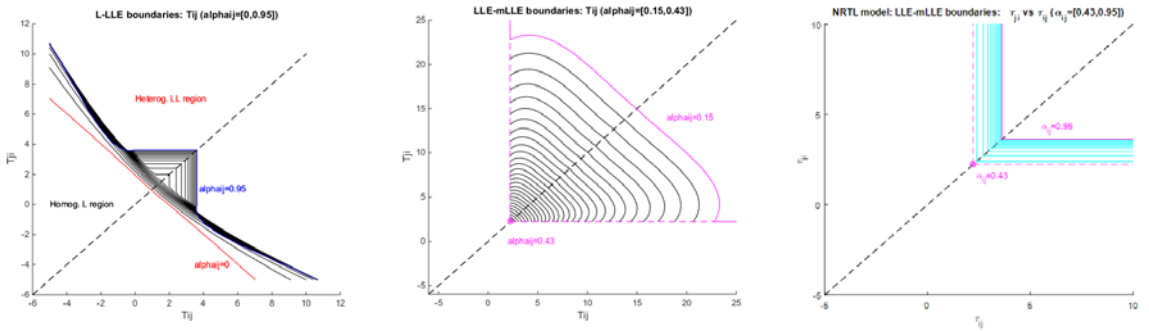


b)

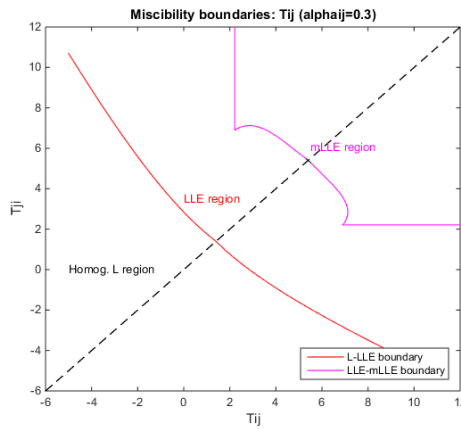
c)



d)



e)

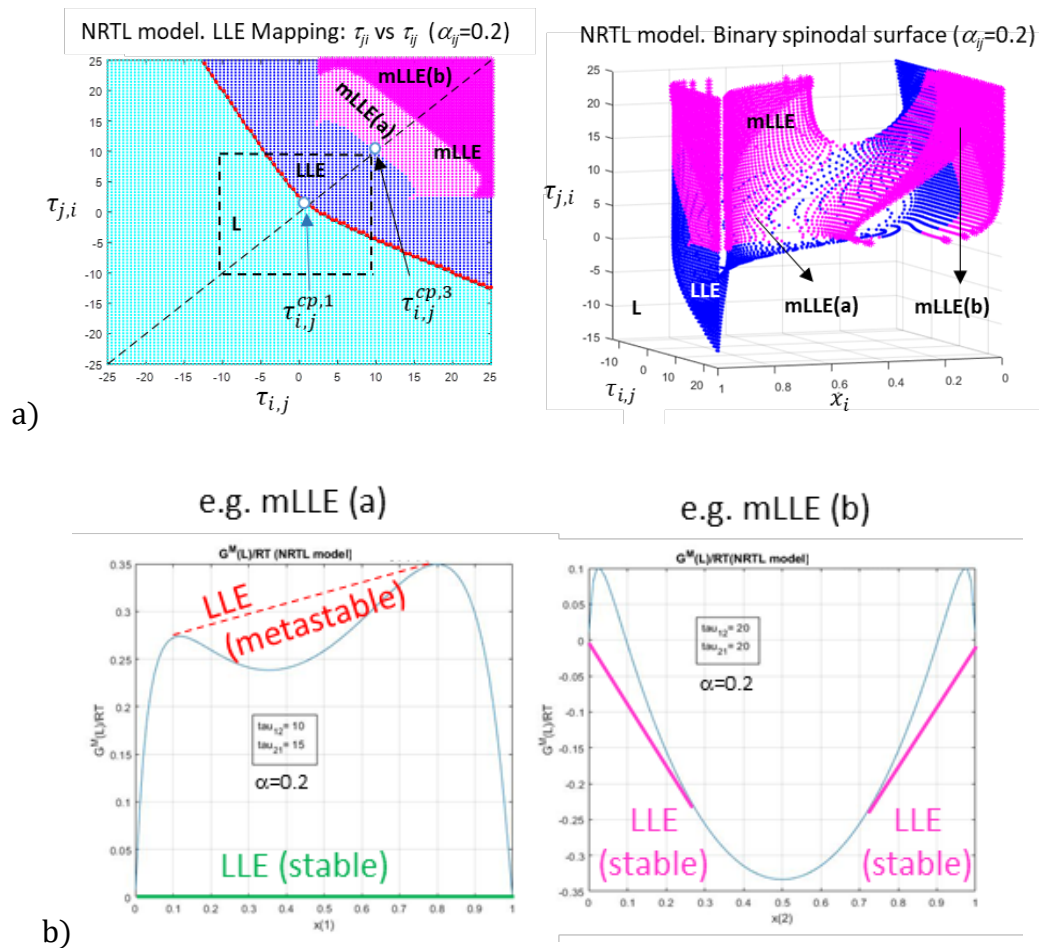


f)

Figure 1. Examples of different individual graphs that can be generated with the GUI developed: Boundaries_LL_NRTL (RUA).

A deeper analysis of the mLLE region for $\alpha_{i,j}=0.2$, indicates that this region presents two different behaviors (see Figure 2a,b): mLLE(a) where one of the LL splittings is metastable and mLLE(b) where both LL splittings are stable (Sapkowski & Hofman, Fluid Phase Equilibria, 2023). In any case, both regions mLLE(a) and (b) present values of the $\tau_{i,j}$ too large (larger than 10) in order to correlate correctly LLE data, especially in multicomponent systems, because e.g. in ternary systems they produce Gibbs energy of mixing functions so flattened that produce too much uncertainty in the solutions obtained.

On the other hand, the region mLLE(a) decreases when the $\alpha_{i,j}$ value increases, and it disappears at an α_{ij} value around 0.45 (Figure 2c).



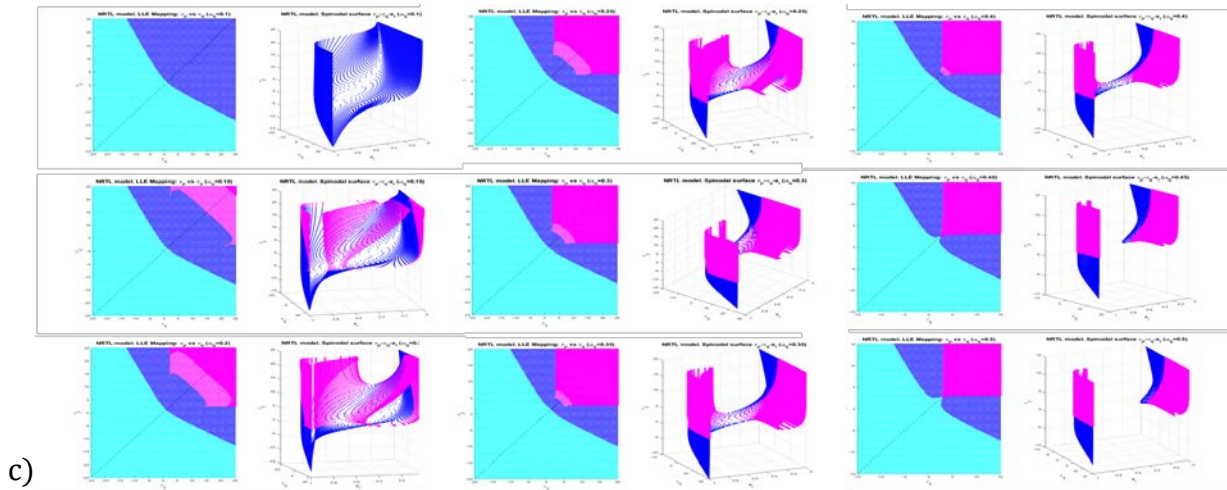
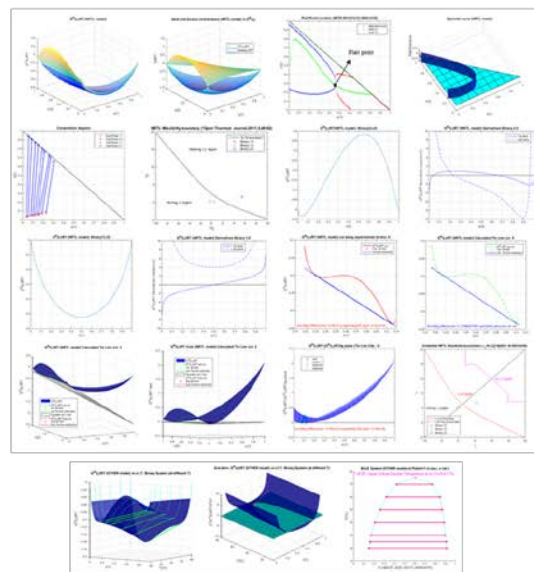


Figure 2. Evolution of the mLLE region with the $\alpha_{i,j}$ value.

For further information or comments: ja.labarta@ua.es
(ORCID ID: <http://orcid.org/0000-0002-4870-2031>)

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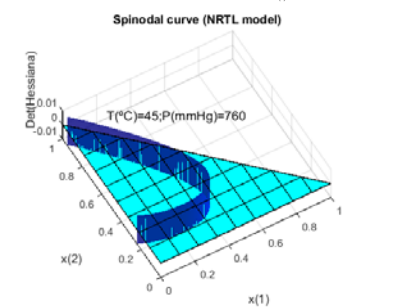
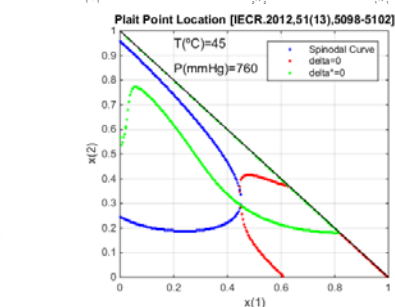
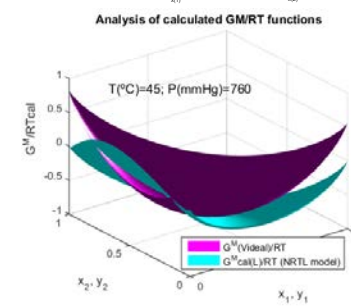
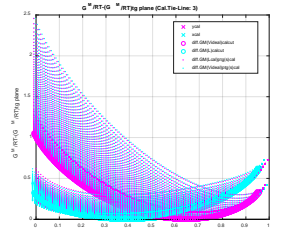
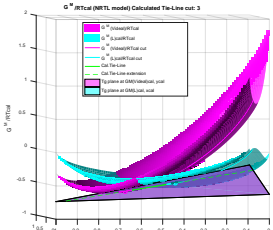
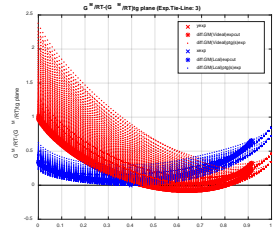
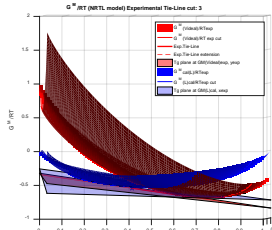
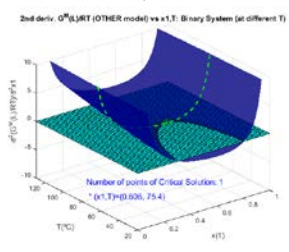
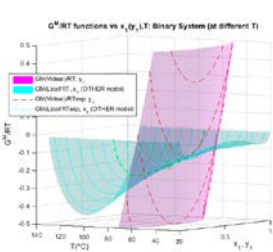
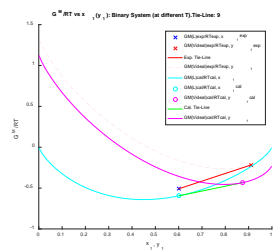
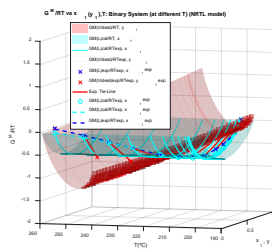
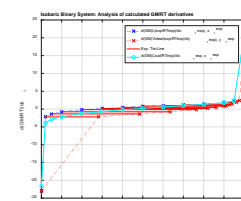
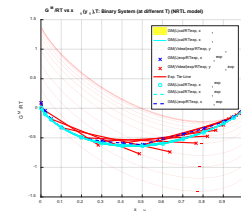
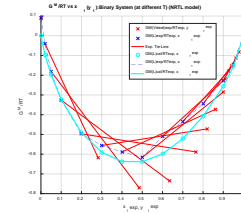
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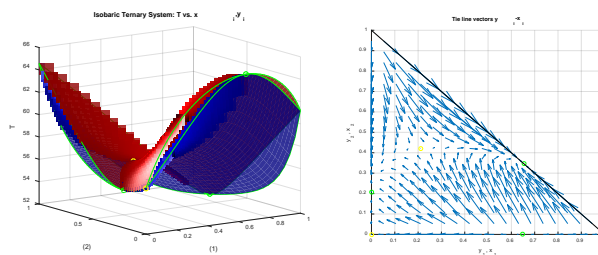
Binary Spinodal Surfaces (in the τ_{ij} - $\tau_{j,i}$ - x_i space), LLE Maps, and Miscibility Boundaries

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[3] Labarta, J.A.; Olaya, M.M.; Marcilla, A. **GMcal_TieLinesVL: Graphical User Interface (GUI) for the Topological Analysis of Experimental and Calculated G^M Functions for Binary and Ternary (isobaric or isothermal) Vapor-Liquid Equilibrium (VLE) data (including Tie-Lines, Derivatives, Distillation Boundaries, LL Critical Points Location, etc.).** Institutional Repository of the University of Alicante (RUA). 2022. Available at: <http://hdl.handle.net/10045/122857>.





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The screenshot displays the ParamIni_LL_NRTL GUI. The main window title is "ParamIni_LL_NRTL". Below the title bar, there is a description: "Graphical User Interface (GUI) for the Selection of NRTL Initial Parameters for the Correlation of Ternary Liquid-Liquid Equilibrium Data (Type I, II, III and 0 (LL island), i.e. with 1, 2, 3 or 0 binary pairs partially miscible) --- NRTL model ---". The user is identified as "Chemical Engineering Department & Institute of Chemical Process Engineering, University of Alicante (Spain)".

The interface includes several sections:

- Data source:** "Introduce Excel file name and press enter: Data_Example1_T1.xls". A "Data Loaded!!" indicator is present.
- System Type (Treybal classification):** A dropdown menu is set to "1".
- Data Base Analysis and suggested initial parameters:** A table with columns for i, j , τ_{ij} , τ_{ji} , and $\alpha_{ij} = \alpha_{ji}$.

i, j	τ_{ij}	τ_{ji}	$\alpha_{ij} = \alpha_{ji}$
1,2	-3.19996	0.700032	0.1
1,3	-3.00044	8.79883	0.0517236
2,3	0.299907	2.00016	0.5
- Buttons:** "Start Composition Diagram Analysis", "Calculate GM(L)RT surfaces with tie-lines", "Calculate Binary GM(L) curves", "Hessian Matrix Determinant & Plait point location", "Calculate Gideal(L)RT and GE(L)RT", "Calculate Gideal(L)RT and GE(L)RT".
- Topological Revision:** "Calculate Gideal(L)RT and GE(L)RT".
- NRTL Binary Parameter Boundaries (τ_{ij} vs τ_{ji}) for Total and Partial Miscibility:** Includes a "Correlated miscibility boundaries" checkbox and a "Number of the Tie-line to represent a GMRT cut: 0 (press enter)".
- Additional bibliography:** A list of references [1] through [12] is provided at the bottom.

On the right side of the GUI, there are three composition diagrams:

- Composition diagram (Test system): 10 Be-lines:** A ternary phase diagram showing 10 blue tie-lines originating from the vertices of the triangle.
- FO and number of tie-lines for each training system:** A scatter plot with two y-axes, showing data points for different training systems.
- Composition diagram (Training system 1): 10 Be-lines:** A ternary phase diagram showing 10 blue tie-lines, similar to the first diagram.

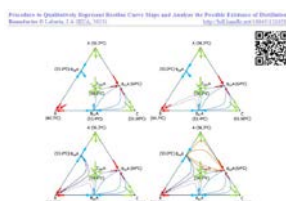
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REMARK: IF YOU WANT TO RECEIVE A NOTIFICATION WITH POSSIBLE UPDATES OF THIS GUI. PLEASE SENT AN E-MAIL TO: ja.labarta@ua.es (ORCID http://orcid.org/0000-0002-4870-2031)